

## **Influence of Slip and Joule Heating on MHD Peristaltic Blood flow with uniform Porous medium through an Inclined asymmetric Vertical Tapered Channel in the presence of Radiation-Blood flow model**

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(Acceptance Date 15th June, 2016)

### **Abstract**

In this article, an influence of slip and joule heating on MHD peristaltic blood flow with uniform porous medium through an inclined asymmetric vertical tapered channel in the presence of radiation -blood flow model have been investigated. The impact of all the physical parameters is plotted for velocity profile, pressure gradient, temperature and heat transfer coefficient. It is notice that the axial velocity increases with increase in  $M$ ,  $\beta$ ,  $\eta$  and  $\alpha$ . We observe that the pressure gradient enhances with increase in  $M$ ,  $\beta$ ,  $\eta$  and  $\alpha$ . However reverse situation is observed for an increase in the values of porous parameter ( $Da$ ) and Volumetric flow rate ( $Q$ ). Further, we notice that the temperature distribution increases with increase in  $M$ ,  $Pr$ ,  $Da$ ,  $N$ ,  $\gamma$  and  $Br$  and also temperature distribution decreases with increase in  $\beta$  and  $\eta$ .

*Key words:* MHD, Joule heating, radiation, porous medium and Inclined channel.

### **1. Introduction**

**T**o the best of our knowledge, no investigation has been made yet to analyze an influence of slip and joule heating on MHD peristaltic blood flow through an inclined asymmetric vertical tapered channel in the

presence of radiation effect-blood flow model. The purpose of the present paper is to provide such an attempt for a MHD Newtonian fluid through porous medium with Joule heating and radiation under the influence of slip conditions. Interest in peristaltic flow has been aroused by its relevance to biological processes, and its potential for industrial and medical applications. The behaviour of most of the physiological fluids, oil, hydrocarbons and polymer are known to be non-Newtonian. One of the major chemical mechanisms for fluid transport in many biological systems is well known to physiologists to be peristalsis. Peristalsis is an important mechanism for mixing and transporting fluids, which is generated by a progressive wave of contraction or expansion moving along a tube. This travelling wave phenomenon is referred to as peristalsis. Peristalsis has its immense applications in medical physiology as well as in industry. In medical physiology, it is involved in the motion of food material in the GIT. In reproductive parts, it helps in the transportation of spermatozoa in the ductus efferentes of the male reproductive tract and in the cervical canal, in the embryo implantation in the fundus site of female uterus and in the movement of an ovum in the fallopian tubes of the female reproductive parts. It also helps in the vasomotion of small blood vessels as well as blood flow in arteries, transport of urine from a kidney to ureter and movement of secretions in glandular ducts (bile and saliva). Some worms also move with the help of peristalsis. Nowadays, peristalsis has exploited its significance in industry, like in sanitary fluid transport, artificial blood pumps in the heart-lung machine and transport of corrosive fluids where the contact of the fluid with the boundary is prohibited. Peristaltic studies are

useful for having a proper understanding of the functioning of different machines used by clinicians for pumping blood and magnetic resonance imaging (MRI). The study of the mechanisms of peristalsis, in both mechanical and physiological situations, has been the object of scientific research for quite some time. Several theoretical and experimental attempts have been done in Latham<sup>12</sup> to find out the peristaltic action in different situations. Mathematical studies of peristalsis were initiated by Fung & Yih<sup>3</sup>, Shapiro *et al.*<sup>25</sup>, and others. Most of these analyses are based on Navier-Stokes equation, considering flow in a circular cylindrical tube or two-dimensional channel with a sinusoidal displacement wave travelling in its wall at a constant velocity. Influence of velocity slip conditions on MHD peristaltic flow of a Prandtl fluid in a non-uniform channel was discussed by Kumar *et al.*<sup>11</sup>. In another attempt, T. Hayat *et al.*<sup>5</sup> studied on an influence of convective conditions in radiative peristaltic flow of pseudo plastic nanofluid in a tapered asymmetric channel. Peristaltic Transport in a Slip Flow has been discussed by Kawang-Hua Chu, W., and Fang, J<sup>7</sup>. In another paper, A.V. Ramana Kumari and G. Radhakrishnamacharya<sup>17</sup> discussed on Effect of slip on peristaltic transport in an inclined channel with wall effects. Afterward, few relevant interested discussions can be seen via attempts such as R.H. Reddy *et al.*<sup>24</sup>, Srinivas, S. *et al.*<sup>27</sup>, S.V.H.N. Krishna Kumari *et al.*<sup>10</sup>, Lika Hummady *et al.*<sup>13</sup>, Ravikumar<sup>19-23</sup>, T. Hayat, M.U. Qureshi and N.Ali<sup>6</sup>, M. Mishra, A. R. Rao<sup>14</sup>.

Heat transfer analysis is prevalent in the study of peristaltic flows due to its large

number of applications in processes like hemodialysis (the method used for removing waste products from blood in the case of renal failure of a kidney) and oxygenation. Bioheat is currently considered as heat transfer in the human body. In view of thermotherapy (application of heat to the body for treatment, examples pain relief, increase of blood flow and others) and human thermoregulation system (ability of living body to maintain body temperature within certain limits in case of surrounding temperature variations) as mentioned by Srinivas and Kothandapani<sup>9</sup>, bioheat transfer has attracted many biomedical experts. Heat transfer analysis is important especially in the case of non-Newtonian peristaltic rheology as there involve many intricate processes like heat conduction in tissues, heat transfer during perfusion (process of delivery of blood to capillary bed) of arterial-venous blood, metabolic heat generation and heat transfer due to some external interactions like mobile phones and radioactive treatments. It is also helpful in the treatment of diseases like the removal of undesirable tissues in cancer. Vajravelu *et al.*<sup>28</sup> have presented a mathematical model for peristaltic flow and heat transfer in a vertical porous annulus with long wave approximation. In another attempt, Nadeem *et al.*<sup>16</sup> discussed on influence of heat transfer in peristalsis with variable viscosity. Sabir Ali Shehzad *et al.*<sup>26</sup> investigated on MHD Mixed Convective Peristaltic Motion of Nanofluid with Joule Heating and Thermophoresis Effects. T.Hayat *et al.*<sup>4</sup> studied on Soret and Dufour effects on peristaltic flow in an asymmetric channel. Mustafa, M<sup>15</sup> has been investigated on mixed convective peristaltic flow of fourth grade fluid with Dufour and Soret effects. Recently, Ravi Kumar<sup>18</sup> investi-

gated on Analysis of Heat Transfer on MHD Peristaltic Blood Flow with Porous Medium through Coaxial Vertical Tapered Asymmetric Channel with Radiation – Blood Flow Study. Some pertinent studies on the present topic can be found from the list of Refs. Such as K. Venugopal Reddy *et al.*<sup>29</sup>, M Kothandapani *et al.*<sup>8</sup>, Sk Abzal *et al.*<sup>1</sup>

## 2. Formulation of the problem :

The model simulates the peristaltic transport of a viscous fluid through an infinite two-dimensional asymmetric vertical tapered channel through the porous medium. Asymmetry in the flow is due to the propagation of peristaltic waves of different amplitudes and phase on the channel walls. We assume that the fluid is subject to a constant transverse magnetic field  $B_0$ . The flow is generated by sinusoidal wave trains propagating with steady speed  $c$  along the tapered asymmetric channel walls<sup>6,20-22</sup>.

The geometry of the wall surface is defined as

$$Y = H_2 = b + m'X + d \sin \left[ \frac{2\pi}{\lambda}(X - ct) \right] \quad (1)$$

$$Y = H_1 = -b - m'X - d \sin \left[ \frac{2\pi}{\lambda}(X - ct) + \phi \right] \quad (2)$$

Where  $b$  is the half-width of the channel,  $d$  is the wave amplitude,  $c$  is the phase speed of the wave and  $m'$  ( $m' \ll 1$ ) is the non-uniform parameter,  $\lambda$  is the wavelength,  $t$  is the time and  $X$  is the direction of wave propagation. The phase difference  $\phi$  varies in the range  $0 \leq \phi \leq \pi$ ,  $\phi = 0$  corresponds to symmetric channel with waves out of phase and further  $b$ ,  $d$  and  $\phi$  satisfy the following conditions for the divergent channel at the inlet

$$d \cos\left(\frac{\phi}{2}\right) \leq b$$

It is assumed that the left wall of the channel is maintained at temperature  $T_0$  while the right wall has temperature  $T_1$ .

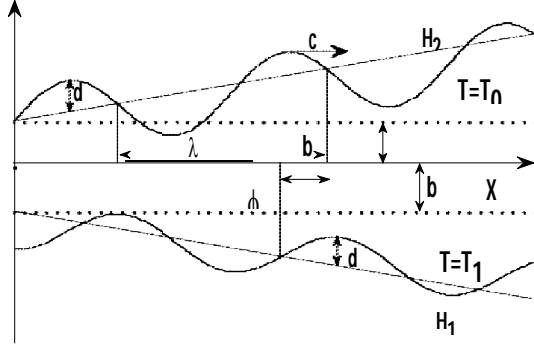


Fig. 1 Schematic diagram of the physical model

The equations governing the motion for the present problem prescribed by  
The continuity equation is

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (3)$$

The movement equations are

$$\rho \left[ u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right] = - \frac{\partial p}{\partial x} + \mu \left[ \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right] - \left[ \sigma B_0^2 \right] (u + c) - \left[ \frac{\mu}{k_1} \right] (u + c) + \rho g \sin \alpha \quad (4)$$

$$\rho \left[ u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right] = - \frac{\partial p}{\partial y} + \mu \left[ \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right] - \left[ \sigma B_0^2 \right] v - \left[ \frac{\mu}{k_1} \right] v - \rho g \cos \alpha \quad (5)$$

The energy equation is

$$\rho C_p \left[ u \frac{\partial}{\partial x} + v \frac{\partial}{\partial y} \right] T = k \left[ \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} \right] T + Q_0 + \sigma B_0^2 u^2 - \frac{\partial q}{\partial y} \quad (6)$$

$u$  and  $v$  are the velocity components in the corresponding coordinates,  $k_1$  is the permeability of the porous medium,  $\rho$  is the density of the fluid,  $p$  is the fluid pressure,  $k$  is the thermal conductivity,  $\mu$  is the coefficient of the viscosity,  $Q_0$  is the constant heat addition/absorption,  $C_p$  is the specific heat at constant pressure,  $\sigma$  is the electrical conductivity,  $g$  is the acceleration due to gravity and  $T$  is the temperature of the fluid.

The relative boundary conditions are

$$\bar{U} = 0, \quad \bar{T} = T_0 \quad \text{at} \quad \bar{Y} = \bar{H}_1$$

$$\bar{U} = 0, \quad \bar{T} = T_1 \quad \text{at} \quad \bar{Y} = \bar{H}_2$$

The radioactive heat flux (Cogley *et al.*<sup>2</sup>) is given by

$$\frac{\partial q}{\partial y} = 4\alpha^2 (T_0 - T_1) \quad (7)$$

here  $\alpha$  is the mean radiation absorption coefficient.

Introducing a wave frame  $(x, y)$  moving with velocity  $c$  away from the fixed frame  $(X, Y)$  by the transformation

$$x = X - ct, \quad y = Y, \quad u = U - c, \quad v = V \quad \text{and} \quad p(x) = P(X, t) \quad (8)$$

Introducing the following non-dimensional quantities:

$$\bar{x} = \frac{x}{\lambda}, \quad \bar{y} = \frac{y}{b}, \quad \bar{t} = \frac{ct}{\lambda}, \quad \bar{u} = \frac{u}{c}, \quad \bar{v} = \frac{v}{c\delta}, \quad h_1 = \frac{H_1}{b}$$

$$h_2 = \frac{H_2}{b}, \quad p = \frac{b^2 p}{c \lambda \mu}, \quad \theta = \frac{T - T_0}{T_1 - T_0}, \quad \delta = \frac{b}{\lambda}$$

$$\text{Re} = \frac{\rho c b}{\mu} N^2 = \frac{4\alpha^2 d_1^2}{k} \varepsilon = \frac{d}{b} \eta = \frac{\rho a_0^2 g}{\mu c} \quad M^2 \delta^2 v - \delta^2 \frac{1}{Da} v - \eta_1 \cos \alpha \quad (11)$$

$$\eta_1 = \frac{\rho a_0^3 g}{\lambda \mu c} \quad (9)$$

where  $\varepsilon = \frac{d}{b}$  is the non-dimensional amplitude

of channel  $\delta = \frac{b}{\lambda}$ , is the wave number,

$k_1 = \frac{\lambda m'}{b}$  is the non-uniform parameter, Re

is the Reynolds number, M is the Hartman

number,  $K = \frac{k}{b^2}$  Permeability parameter, Pr

is the Prandtl number,  $E_c$  is the Eckert number,  $\gamma$  is the heat source/sink parameter,  $B_r (= E_c P_r)$  is the Brinkman number,  $\eta$  and  $\eta_1$  are gravitational parameters and  $N^2$  is the radiation parameter.

### 3. Solution of the problem :

In view of the above transformations (8) and non-dimensional variables (9), equations (3-6) are reduced to the following non-dimensional form after dropping the bars

$$\text{Re} \delta \left[ u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right] = \left( -\frac{\partial p}{\partial x} + \delta^2 \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} - Au - A + \eta \sin \alpha \right) \quad (10)$$

$$\text{Re} \delta^3 \left[ u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right] = \left( -\frac{\partial p}{\partial y} + \delta^4 \frac{\partial^2 v}{\partial x^2} + \delta^2 \frac{\partial^2 v}{\partial y^2} - \right.$$

$$\left. \text{Re} \left[ \delta u \frac{\partial \theta}{\partial x} + v \delta \frac{\partial \theta}{\partial y} \right] = \frac{1}{\text{Pr}} \left[ \delta^2 \frac{\partial^2 \theta}{\partial x^2} + \frac{\partial^2 \theta}{\partial y^2} \right] + \beta + \right.$$

$$\left. M^2 E u^2 + \frac{N^2 \theta}{P_r} \right) \quad (12)$$

Applying long wave length approximation and neglecting the wave number along with low-Reynolds numbers. Equations (10-12) become

$$\frac{\partial^2 u}{\partial y^2} - Au = \frac{\partial p}{\partial x} + A - \eta \sin \alpha \quad (13)$$

$$\frac{\partial p}{\partial y} = 0 \quad (14)$$

$$\frac{1}{\text{Pr}} \left[ \frac{\partial^2 \theta}{\partial y^2} \right] + \beta + M^2 E u^2 + \frac{N^2 \theta}{P_r} = 0 \quad (15)$$

$$\text{Where } A = \left( M^2 + \frac{1}{Da} \right)$$

The relative boundary conditions in dimensionless form are given by

$$u = -\beta \frac{\partial u}{\partial y}, \quad \theta = 0 \quad \text{at } y = h_1 \quad (16)$$

$$u = \beta \frac{\partial u}{\partial y}, \quad \theta = 1 \quad \text{at } y = h_2 \quad (17)$$

Where

$$h_1 = -1 - k_1 x - \varepsilon \sin[2\pi(x-t) + \phi]$$

$$h_2 = 1 + k_1 x + \varepsilon \sin[2\pi(x-t)]$$

Where  $\beta$  is the non-dimensional slip velocity parameter.

The solutions of velocity and temperature with

subject to boundary conditions (16) and (17) are given by

$$u = G \sin h[\alpha y] + H \cos h[\alpha y] + F \quad (18)$$

Where

$$\alpha = \sqrt{\left(M^2 + \frac{1}{Da}\right)}$$

$$F = \frac{D}{M^2 D + 1} \left( \eta \sin \alpha - \frac{\partial p}{\partial x} \right) - 1$$

$$G = \left( \frac{-F \left( \frac{a_1}{a_2} \right) (\cos h[\alpha h_1] + \beta \alpha \sin h[\alpha h_1]) - F}{\sin h[\alpha h_1] + \beta \alpha \cos h[\alpha h_1]} \right)$$

$$H = \left( \frac{F a_1}{a_2} \right)$$

$$a_1 = \left( \left( \frac{\sin h[\alpha h_2] - \beta \alpha \cos h[\alpha h_2]}{\sin h[\alpha h_1] + \beta \alpha \cos h[\alpha h_1]} \right) - 1 \right)$$

$$a_2 = - \left( \frac{\cos h[\alpha h_1] + \beta \alpha \sin h[\alpha h_1]}{\sin h[\alpha h_1] + \beta \alpha \cos h[\alpha h_1]} \right) *$$

$$(\sin h[\alpha h_2] - \beta \alpha \cos h[\alpha h_2]) +$$

$$(\cos h[\alpha h_2] - \beta \alpha \sin h[\alpha h_2])$$

$$\theta = J \cos[Ny] + K \sin[Ny] - \left( \frac{P_r \gamma}{N^2} \right) - \left( \frac{M^2 B_r a_3}{4\alpha^2 + N^2} e^{2\alpha y} \right) -$$

$$\left( \frac{M^2 B_r a_4}{4\alpha^2 + N^2} e^{-2\alpha y} \right) - \left( \frac{M^2 B_r a_5}{\alpha^2 + N^2} e^{\alpha y} \right) - \left( \frac{M^2 B_r a_6}{\alpha^2 + N^2} e^{-\alpha y} \right) -$$

$$\left( \frac{M^2 B_r a_7}{N^2} \right)$$

Where

$$J = \frac{-K \sin[N h_1] + \left( \frac{P_r \gamma}{N^2} \right) + \left( \frac{M^2 B_r a_3}{4\alpha^2 + N^2} e^{2\alpha h_1} \right)}{\cos[N h_1]} +$$

$$\left( \frac{M^2 B_r a_4}{4\alpha^2 + N^2} e^{-2\alpha h_1} \right) + \left( \frac{M^2 B_r a_5}{\alpha^2 + N^2} e^{\alpha h_1} \right) \frac{1}{\cos[N h_1]} +$$

$$\left( \frac{M^2 B_r a_6}{\alpha^2 + N^2} e^{-\alpha h_1} \right) + \left( \frac{M^2 B_r a_7}{N^2} \right) \frac{1}{\cos[N h_1]}$$

$$K = \left( \frac{-\left( \frac{P_r \gamma}{N^2} \right) (\cos[N h_1] - \cos[N h_2])}{\sin[N h_1] \cos[N h_2] - \sin[N h_2] \cos[N h_1]} \right) -$$

$$\left( \frac{M^2 B_r a_3}{4\alpha^2 + N^2} (e^{2\alpha h_2} \cos[N h_1] - e^{2\alpha h_1} \cos[N h_2]) \right) \frac{1}{\sin[N h_1] \cos[N h_2] - \sin[N h_2] \cos[N h_1]} -$$

$$\left( \frac{M^2 B_r a_4}{4\alpha^2 + N^2} (e^{-2\alpha h_2} \cos[N h_1] - e^{-2\alpha h_1} \cos[N h_2]) \right) \frac{1}{\sin[N h_1] \cos[N h_2] - \sin[N h_2] \cos[N h_1]} -$$

$$\left( \frac{M^2 B_r a_5}{\alpha^2 + N^2} (e^{\alpha h_2} \cos[N h_1] - e^{\alpha h_1} \cos[N h_2]) \right) \frac{1}{\sin[N h_1] \cos[N h_2] - \sin[N h_2] \cos[N h_1]} -$$

$$\left( \frac{M^2 B_r a_6}{\alpha^2 + N^2} (e^{-\alpha h_2} \cos[N h_1] - e^{-\alpha h_1} \cos[N h_2]) \right) \frac{1}{\sin[N h_1] \cos[N h_2] - \sin[N h_2] \cos[N h_1]} -$$

$$\left( \frac{M^2 B_r a_7}{N^2} (\cos[N h_1] - \cos[N h_2]) \right) \frac{1}{\sin[N h_1] \cos[N h_2] - \sin[N h_2] \cos[N h_1]} -$$

$$\left( \frac{\cos[N h_1]}{\sin[N h_1]\cos[N h_2] - \sin[N h_2]\cos[N h_1]} \right)$$

$$a_3 = \left( \frac{G^2}{4} + \frac{H^2}{4} + \frac{GH}{2} \right) a_4 = \left( \frac{G^2}{4} + \frac{H^2}{4} - \frac{GH}{2} \right)$$

$$a_5 = F(G + H) \quad a_6 = F(H - G)$$

$$a_7 = \left( -\frac{G^2}{2} + \frac{H^2}{2} + F^2 \right)$$

The coefficients of the heat transfer  $Zh_1$  and  $Zh_2$  at the walls  $y = h_1$  and  $y = h_2$  respectively, are given by

$$Zh_1 = \theta_y h_{1x} \quad (20)$$

$$Zh_2 = \theta_y h_{2x} \quad (21)$$

The solutions of the coefficient of heat transfer at  $y = h_1$  and  $y = h_2$  are given by

$$Zh_1 = \theta_y h_{1x} =$$

$$\left( -J N \sin[N y] + K N \cos[N y] - \left( \frac{2\alpha M^2 B_r a_3}{4\alpha^2 + N^2} e^{2\alpha y} \right) - \right.$$

$$\left( \frac{-2\alpha M^2 B_r a_4}{4\alpha^2 + N^2} e^{-2\alpha y} \right) - \left( \frac{\alpha M^2 B_r a_5}{\alpha^2 + N^2} e^{\alpha y} \right) +$$

$$\left( \frac{\alpha M^2 B_r a_6}{\alpha^2 + N^2} e^{-\alpha y} \right) \left( -2\pi \varepsilon \cos[2\pi(x-t) + \phi] - k_1 \right)$$

$$Zh_2 = \theta_y h_{2x} =$$

$$\left( -J N \sin[N y] + K N \cos[N y] - \left( \frac{2\alpha M^2 B_r a_3}{4\alpha^2 + N^2} e^{2\alpha y} \right) - \right.$$

$$\left( \frac{-2\alpha M^2 B_r a_4}{4\alpha^2 + N^2} e^{-2\alpha y} \right) - \left( \frac{\alpha M^2 B_r a_5}{\alpha^2 + N^2} e^{\alpha y} \right) +$$

$$\left( \frac{\alpha M^2 B_r a_6}{\alpha^2 + N^2} e^{-\alpha y} \right) \left( 2\pi \varepsilon \cos[2\pi(-t+x)] + k_1 \right)$$

The volumetric flow rate in the wave frame is defined by

$$q = \int_{h_1}^{h_2} u dy =$$

$$\left( \frac{G}{\alpha} \right) (\cos h[\alpha h_2] - \cos h[\alpha h_1]) + \left( \frac{H}{\alpha} \right) (\sin h[\alpha h_2] - \sin h[\alpha h_1]) + F(h_2 - h_1) \quad (24)$$

The pressure gradient obtained from equation (24) can be expressed as

$$\frac{dp}{dx} = \left( \frac{-qA}{B} \right) + (\eta \sin \alpha - A) \quad (25)$$

Where

$$B = \left( \frac{-1}{\alpha} \right) \left( \frac{\left( \frac{a_1}{a_2} \right) (\cosh[\alpha h_1] + \beta \alpha \sinh[\alpha h_1]) + 1}{\sinh[\alpha h_1] + \beta \alpha \cosh[\alpha h_1]} \right)^* (\cosh[\alpha h_2] - \cosh[\alpha h_1]) + \left( \frac{a_1}{\alpha a_2} \right) (\sinh[\alpha h_2] - \sinh[\alpha h_1]) + (h_2 - h_1)$$

The instantaneous flux  $Q(x, t)$  in the laboratory frame is

$$Q = \int_{h_2}^{h_1} (u + 1) dy = q - h \quad (26)$$

The average volume flow rate over one wave

period ( $T = \lambda/c$ ) of the peristaltic wave is defined as

$$\bar{Q} = \frac{1}{T} \int_0^T Q dt = q + 1 + d \quad (27)$$

From the equations (25) and (27), the pressure gradient can be expressed as

$$\frac{dp}{dx} = \left( \frac{-(\bar{Q} - 1 - d)A}{B} \right) + (\eta \sin \alpha - A) \quad (28)$$

#### 4. Discussion of the problem

The main object of this investigation has been to study an influence of slip and joule heating on MHD peristaltic blood flow with uniform porous medium through an inclined asymmetric vertical tapered channel in the presence of radiation -blood flow model. The analytical expressions for velocity distribution, pressure gradient, and temperature and heat transfer coefficient have been derived in the previous section. The numerical and computational results are discussed through the graphical illustration. **Mathematica** software is used to find out numerical results.

Influence of Hartman number on velocity distribution can be seen through Fig. 2. It was evident that the axial velocity increases with increase in  $M$  ( $M = 1, 1.5, 2$ ) being fixed  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $dp/dx = 0.5$ . Fig. 3 illustrates the variation in an axial velocity for different values of slip parameter  $\beta$  ( $\beta = 0.7, 0.8, 0.9$ ) with fixed  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $dp/dx = 0.5$ . This figure reveals that the axial velocity increases when slip parameter  $\beta$  increased. Fig. 4 depicts that the

axial velocity distribution ( $u$ ) with various values of  $Da$  ( $Da = 0.1, 0.2, 0.3$ ) with fixed other parameters. It is interested to note that the axial velocity decreases with increase in porosity parameter ( $Da$ ). Effect of gravitational parameter ( $\eta$ ) on axial velocity distribution ( $u$ ) shown in figure 5 with  $\beta = 0.7$ ,  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $dp/dx = 0.5$ . We observe from this graph that the axial velocity gradually increases when increase in  $\eta$ . Fig. 6 reveals that the various values of inclined angle  $\alpha$  ( $\alpha = 0, \pi/6, \pi/3$ ) on axial velocity distribution ( $u$ ). It has been inferred that the axial velocity slowly increases by increase in  $\alpha$  being fixed  $\beta = 0.7$ ,  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $dp/dx = 0.5$ . Hence, we notice that the axial velocity increases in the entire tapered channel when an increase in  $M$ ,  $\beta$ ,  $\eta$  and  $\alpha$  (see fig. 2, 3, 5 and 6) and also we observe that the axial velocity decreases in the entire tapered channel when increasing in  $Da$  (see fig. 4).

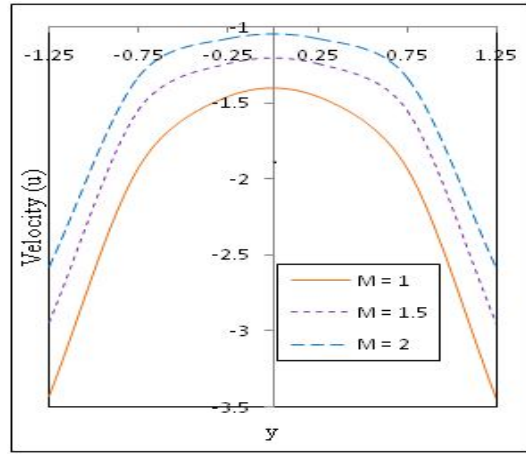


Figure (2): Velocity for different values of  $M$  with fixed  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $dp/dx = 0.5$ .

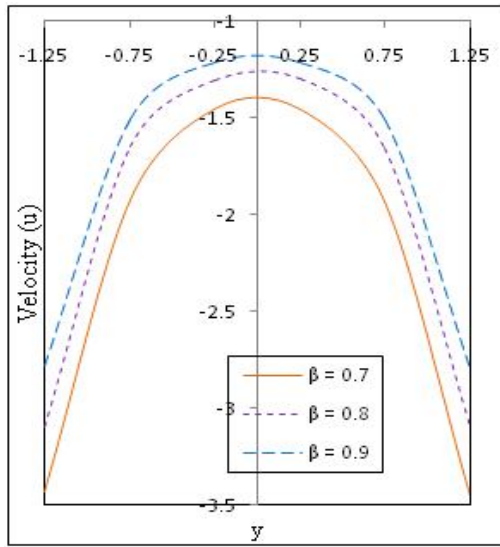


Figure (3): Velocity for different values of  $\beta$  with fixed  $Da=0.3, \phi=\pi/6, \alpha=\pi/6, \eta=0.5, M=1, \dot{a}=0.2, k_1=0.1, x=0.6, t=0.4, dp/dx=0.5$

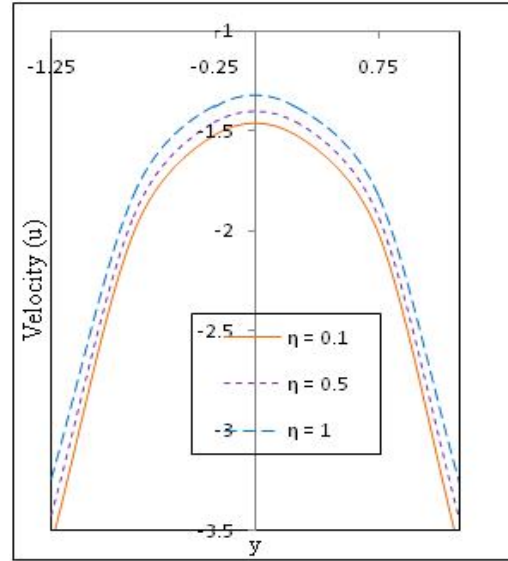


Figure (5): Velocity for different values of  $\eta$  with fixed  $\beta=0.7, Da=0.3, \phi=\pi/6, \alpha=\pi/6, M=1, \dot{a}=0.2, k_1=0.1, x=0.6, t=0.4, dp/dx=0.5$ .

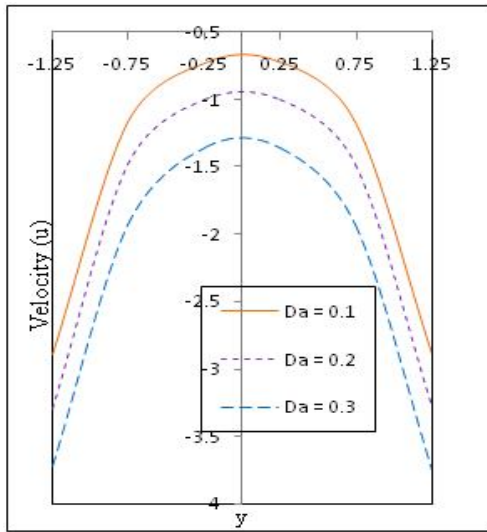


Figure (4): Velocity for different values of  $Da$  with fixed  $\beta=0.7, \phi=\pi/6, \alpha=\pi/6, \eta=0.5, M=1, \varepsilon=0.2, k_1=0.1, x=0.6, t=0.4, dp/dx=0.5$ .

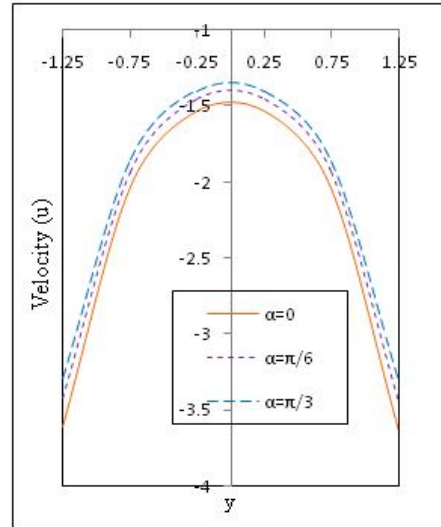


Figure (6): Velocity for different values of  $\alpha$  with fixed  $\beta=0.7, Da=0.3, \phi=\pi/6, \eta=0.5, M=1, \varepsilon=0.2, k_1=0.1, x=0.6, t=0.4, dp/dx=0.5$ .

Fig. 7 illustrates the variation in axial pressure gradient for different values of the Hartmann number  $M$  ( $M = 1, 1.5, 2$ ) with  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\mu = 0.2$ ,  $d = 2$ . This figure reveals as the values of the Hartmann number increases the magnitude of the axial pressure gradient also increases. It shows that when a strong magnetic field is applied to the flow field then higher pressure gradient is needed to pass the flow. An important result depicted in Fig. 8 that the variation in axial pressure gradient for different values of slip parameter  $\beta$  ( $\beta = 0.7, 0.8, 0.9$ ) with  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ . It shows that in the wider part of channel *i.e.*  $x \in (0, 0.3) \cup (0.7, 1)$  the pressure gradient is relatively small. Hence, the flow can easily pass without imposing more pressure gradient. Similarly in the narrow part of channel *i.e.*  $x \in (0.3, 0.7)$ , the flow cannot pass easily. Therefore, it requires more pressure gradient is needed to maintain the same flux to pass through it and also we observe that the axial pressure gradient increases by the increase in  $\beta$ . The axial pressure gradient for different values of porous parameter  $Da$  ( $Da = 0.1, 0.2, 0.3$ ) is plotted in Fig. 9. It can be seen that the axial pressure gradient decreases when porous parameter increased. The influence of gravitational parameter ( $\eta$ ) on axial pressure gradient is presented in Fig. 10. Indeed, the axial pressure gradient is increases by increase in  $\eta$  ( $\eta = 0.1, 0.5, 1$ ) with fixed  $Da = 0.3$ ,  $\beta = 0.7$ ,  $\bar{Q} = \pi/6$ ,  $\alpha = \pi/6$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\mu = 0.2$ ,  $d = 2$ . Fig.11. shows that the effect of inclined angle  $\alpha$  on axial pressure gradient with fixed  $Da = 0.3$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ . We observe from this figure that

the increasing the values of  $\alpha$  ( $\alpha = 0, \pi/6, \pi/3$ ), the results in the flow field increases. Effect of volumetric flow rate ( $\bar{Q}$ ) on axial pressure gradient is depicted in Fig. 12. We notice that the axial pressure gradient decreases by increasing the values of  $\bar{Q}$  ( $\bar{Q} = 0.2, 0.4, 0.6$ ) with  $Da = 0.3$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $d = 2$ .

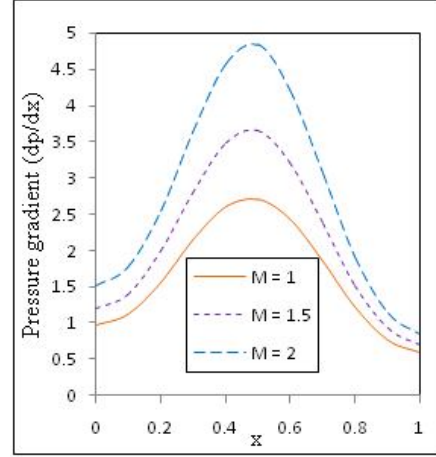


Figure (7): Pressure gradient ( $dp/dx$ ) for different values of  $M$  with fixed  $Da = 0.3$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ .

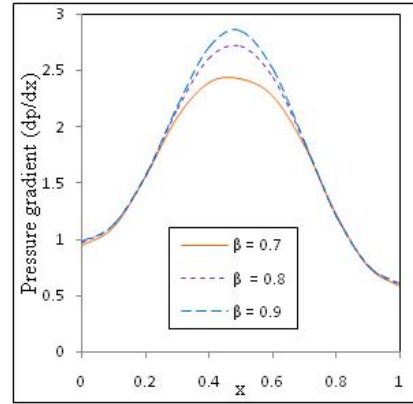


Figure (8): Pressure gradient ( $dp/dx$ ) for different values of  $\beta$  with fixed  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ .

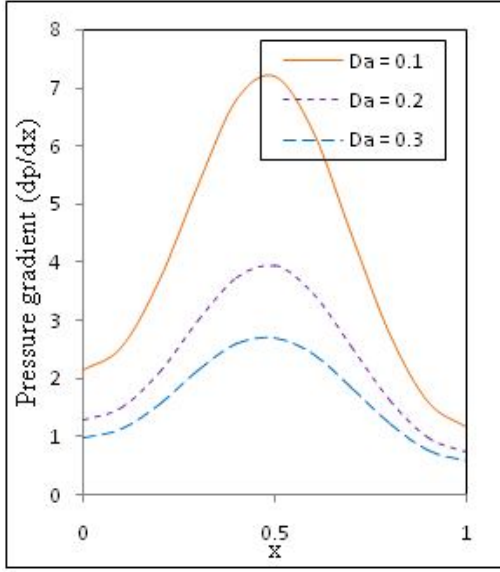


Figure (9): Pressure gradient ( $dp/dx$ ) for different values of  $Da$  with fixed  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ .

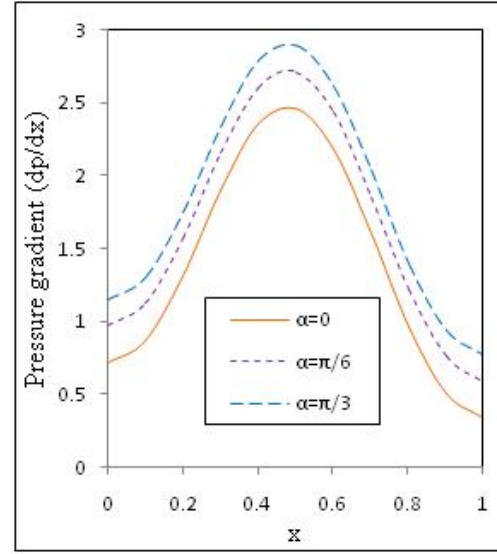


Figure (11): Pressure gradient ( $dp/dx$ ) for different values of  $\alpha$  with fixed  $Da = 0.3$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ .

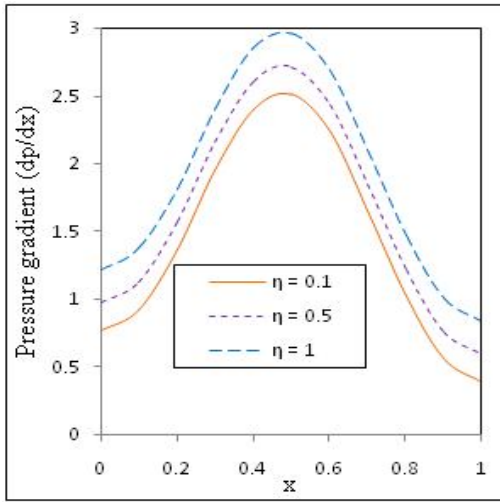


Figure (10): Pressure gradient ( $dp/dx$ ) for different values of  $\eta$  with fixed  $Da = 0.3$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $\bar{Q} = 0.2$ ,  $d = 2$ .

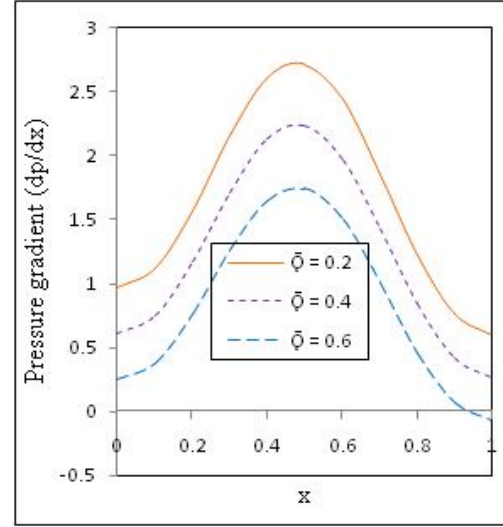


Figure (12): Pressure gradient ( $dp/dx$ ) for different values of  $\alpha$  with fixed  $Da = 0.3$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = \pi/4$ ,  $d = 2$ .

Figure (13) shows that the temperature distribution ( $\theta$ ) for different values of Hartmann number increases ( $M = 1, 1.5, 2$ ) with  $Da = 0.3$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . It was evident that the temperature distribution increases as increase in  $M$ . Figure (14) shows the variation slip parameter  $\beta$  ( $\beta = 0.7, 0.8, 0.9$ ) on temperature ( $\theta$ ) with  $Da = 0.3$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . It can be noticed that from this graph that the temperature of the fluid decreases due to increment in the slip parameter. Effect of porosity parameter  $Da$  ( $Da = 0.1, 0.2, 0.3$ ) on temperature distribution ( $\theta$ ) is plotted in fig 15. We notice that the temperature distribution increases when increase in  $Da$  with fixed  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . Fig. 16 reveals the different of radiation parameter  $N$  ( $N = 0.5, 0.7, 0.9$ ) on temperature profile ( $\theta$ ) with  $Da = 0.3$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . This figure indicates that the temperature distribution enhances when radiation parameter increased. Fig.17 presents the various values of Prandtl number  $Pr$  ( $Pr = 1, 3, 5$ ) on temperature profile with fixed  $Da = 0.3$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . It is obvious that the temperature distribution increases with increase in Prandtl number. Fig.18 depicts the temperature distribution ( $\theta$ ) with different values of Brinkman number  $Br$  ( $Br = 0.1, 0.2, 0.3$ ) with  $Da = 0.3$ ,  $Pr = 1$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x =$

$0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . It was evident from the figure that the temperature distribution increases as increase in  $Br$ . The relation between temperature distribution ( $\theta$ ) and gravitational parameter ( $\eta$ ) is shown in Fig. (19). It is clear that the temperature distribution decreases as  $\eta$  increases being fixed other parameters. Influence of various values heat source/sink parameter  $\gamma$  ( $\gamma = 0.1, 0.3, 0.5$ ) on temperature distribution is presented in Fig.20 with fixed  $Da = 0.3$ ,  $Pr = 1$ ,  $N = 0.5$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ . This figure reveals that the temperature distribution increases as increase in  $\gamma$ .

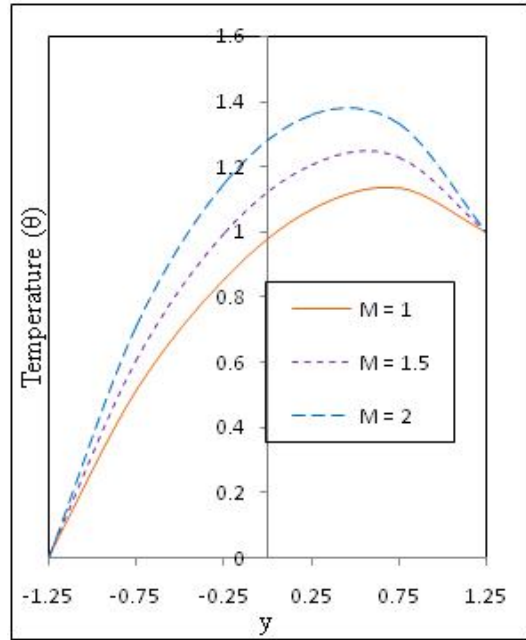


Figure (13): Temperature ( $\theta$ ) for different values of  $M$  with fixed  $Da = 0.3$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

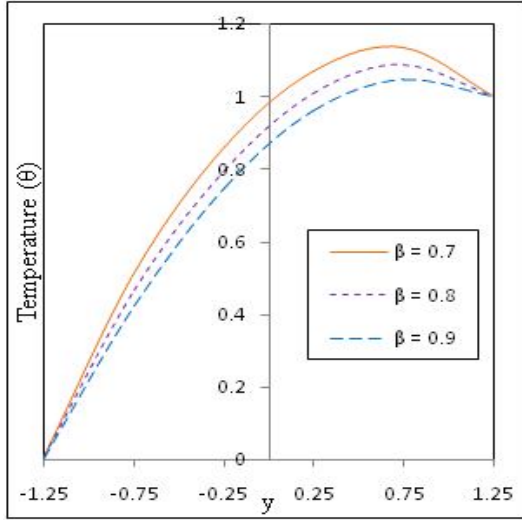


Figure (14): Temperature ( $\theta$ ) for different values of  $\beta$  with fixed  $Da = 0.3$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

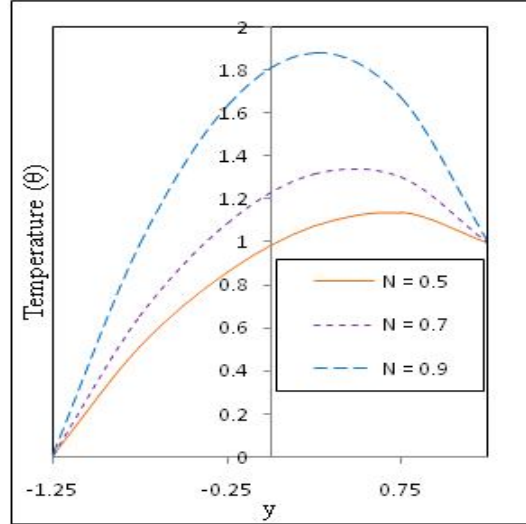


Figure (16): Temperature ( $\theta$ ) for different values of  $N$  with fixed  $Da = 0.3$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

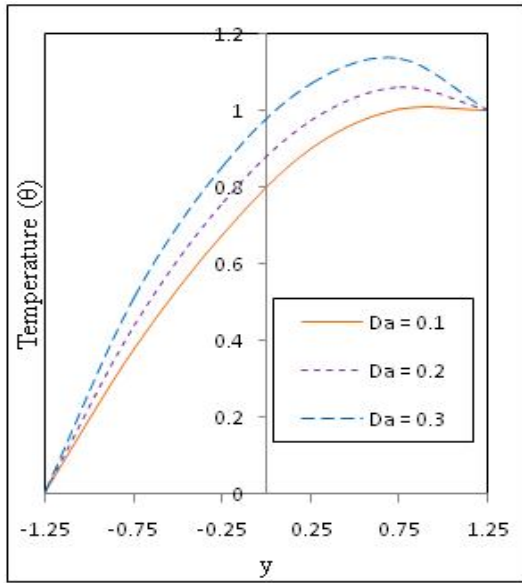


Figure (15): Temperature ( $\theta$ ) for different values of  $Da$  with fixed  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

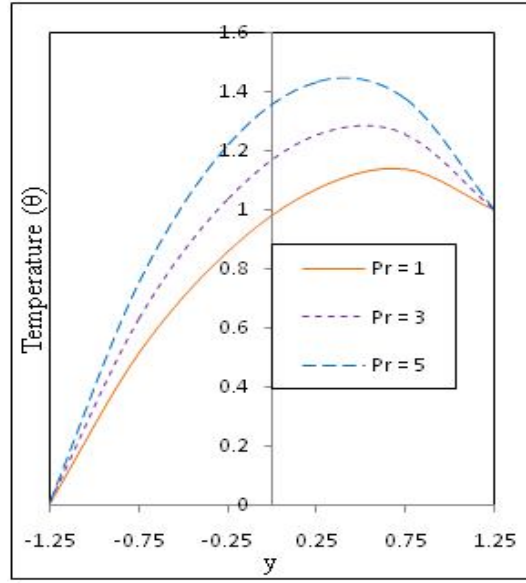


Figure (17): Temperature ( $\theta$ ) for different values of  $Pr$  with fixed  $Da = 0.3$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

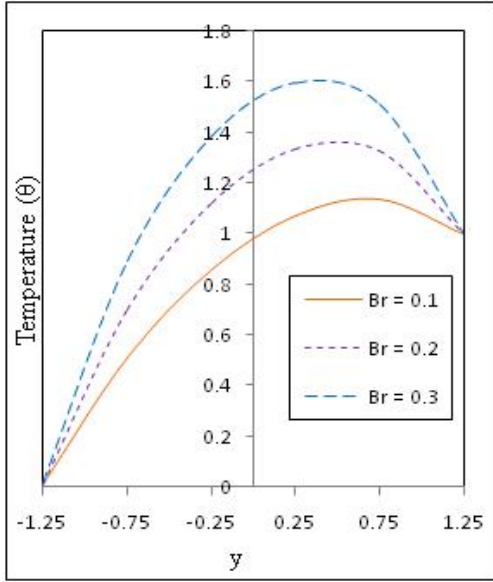


Figure (18): Temperature ( $\theta$ ) for different values of  $Br$  with fixed  $Da = 0.3$ ,  $Pr = 1$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

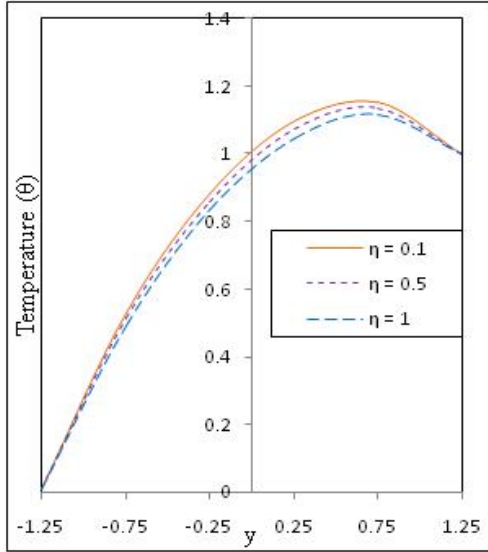


Figure (19): Temperature ( $\theta$ ) for different values of  $\eta$  with fixed  $Da = 0.3$ ,  $Pr = 1$ ,  $N = 0.5$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

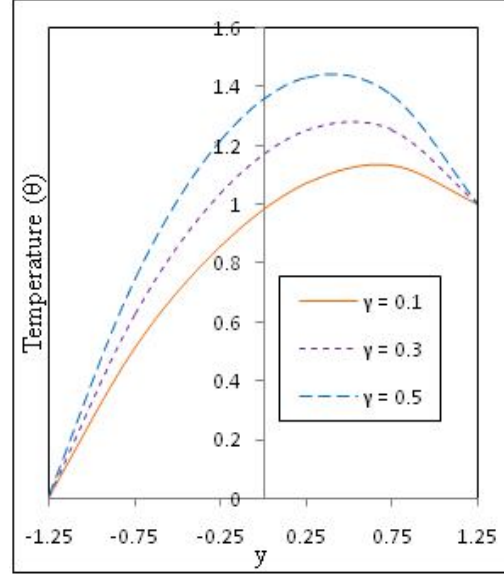


Figure (20): Temperature ( $\theta$ ) for different values of  $\gamma$  with fixed  $Da = 0.3$ ,  $Pr = 1$ ,  $N = 0.5$ ,  $\eta = 0.5$ ,  $M = 1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $x = 0.6$ ,  $t = 0.4$ ,  $p = 0.5$ .

The influence of Hartmann number  $M$  on heat transfer coefficient at the wall  $y = h_1$  is depicted in Fig. 21 with  $Da = 0.3$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\beta = 0.7$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$ . It is obvious that the heat transfer coefficient increases in the portion of the inclined tapered channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it is decreases in the other portion of the inclined tapered channel  $x \in [0.05, 0.58]$  with increase in  $M$  ( $M = 1, 1.5, 2$ ). Fig. 22 presents the heat transfer coefficient with slip parameter being fixed  $Da = 0.3$ ,  $M = 1$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$ . It was evident that from the graph that the heat transfer coefficient decreases in the portion of the inclined tapered channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it is

increases in the other portion of the inclined tapered channel  $x \in [0.05, 0.58]$  as increase in  $\beta$  ( $\beta = 0.7, 0.8, 0.9$ ). Fig. 23 depicts the heat transfer coefficient at the wall  $y = h_1$  for different values of porosity parameter  $Da$  ( $Da = 0.1, 0.2, 0.3$ ) with  $M = 1, N = 0.5, Pr = 1, \gamma = 0.1, Br = 0.1, \beta = 0.7, \phi = \pi/6, \alpha = \pi/6, \eta = 0.5, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$ . It is clear that the heat transfer coefficient increases in the portion of the inclined tapered channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it decreases in the other portion of the inclined tapered channel  $x \in [0.05, 0.58]$  with increase in  $Da$ . The heat transfer coefficient at the wall  $y = h_1$  for various values of radiation parameter  $N$  ( $N = 0.5, 0.7, 0.9$ ) is plotted in Fig. 24 with fixed  $M = 1, Da = 0.3, Pr = 1, \gamma = 0.1, Br = 0.1, \beta = 0.7, \phi = \pi/6, \alpha = \pi/6, \eta = 0.5, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$ . We notice that the heat transfer coefficient increases in the portion of the channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it decreases in the other portion of the channel  $x \in [0.05, 0.58]$  with increase in  $N$ . The effect of Prandtl number  $Pr$  on heat transfer coefficient at the wall  $y = h_1$  with  $M = 1, Da = 0.3, N = 0.5, \gamma = 0.1, Br = 0.1, \beta = 0.7, \phi = \pi/6, \alpha = \pi/6, \eta = 0.5, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$  is shown in Fig. 25. We observe that from this graph that the heat transfer coefficient increases in the portion of the channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it decreases in the rest of the channel  $x \in [0.05, 0.58]$  with increase in  $Pr$  ( $Pr = 1, 3, 5$ ). Fig. 26 shows that the variation in heat transfer coefficient at the wall  $y = h_1$  for different values of Brinkman number  $Br$  ( $Br = 0.1, 0.2, 0.3$ ) with fixed  $M = 1, Da = 0.3, N = 0.5, \gamma = 0.1, Pr = 1, \beta = 0.7, \phi = \pi/6, \alpha = \pi/6, \eta = 0.5, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$ . We notice that the heat transfer coefficient increases in the portion of

the channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it decreases in the rest of the channel  $x \in [0.05, 0.58]$  with increase in  $Br$ . Heat transfer coefficient at the wall  $y = h_1$  for different values of gravitational parameter ( $\eta$ ) with  $M = 1, Da = 0.3, N = 0.5, \gamma = 0.1, Pr = 1, Br = 0.1, \beta = 0.7, \phi = \pi/6, \alpha = \pi/6, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$  as plotted in fig. 27. Indeed, the heat transfer coefficient decreases in the portion of the inclined tapered channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it increases in the other portion of the inclined tapered channel  $x \in [0.05, 0.58]$  as increase in  $\eta$  ( $\eta = 0.1, 0.5, 1$ ). The heat transfer coefficient at the wall  $y = h_1$  for various values of heat source/sink parameter  $\gamma$  ( $\gamma = 0.1, 0.3, 0.5$ ) is presented in Fig. 28 with  $M = 1, Da = 0.3, N = 0.5, Pr = 1, Br = 0.1, \beta = 0.7, \eta = 0.5, \phi = \pi/6, \alpha = \pi/6, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$ . It was evident that the heat transfer coefficient increases in the portion of the channel  $x \in [0, 0.05] \cup [0.58, 1]$  and it decreases in the rest of the channel  $x \in [0.05, 0.58]$  as increase in  $\gamma$ .

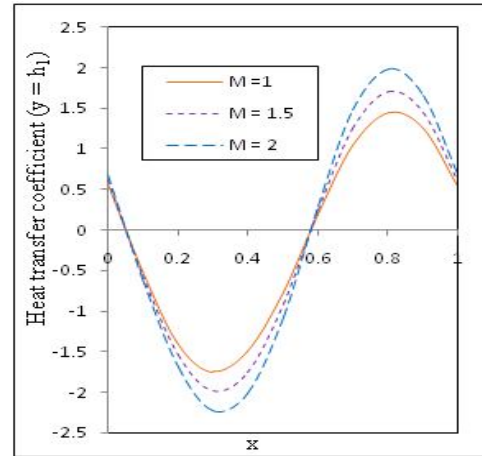


Figure (21): Heat transfer coefficient ( $y = h_1$ ) for different values of  $M$  with fixed  $Da = 0.3, N = 0.5, Pr = 1, \gamma = 0.1, Br = 0.1, \phi = \pi/6, \alpha = \pi/6, \eta = 0.5, \beta = 0.7, \varepsilon = 0.2, k_1 = 0.1, t = 0.4, p = 0.5$

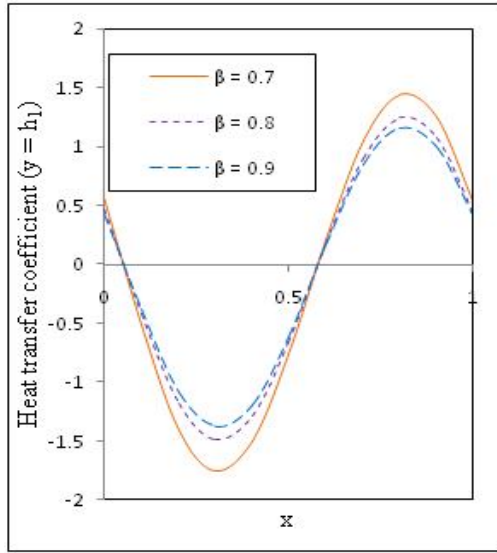


Figure (22): Heat transfer coefficient ( $y = h_1$ ) for different values of  $\beta$  with fixed  $Da = 0.3$ ,  $M = 1$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

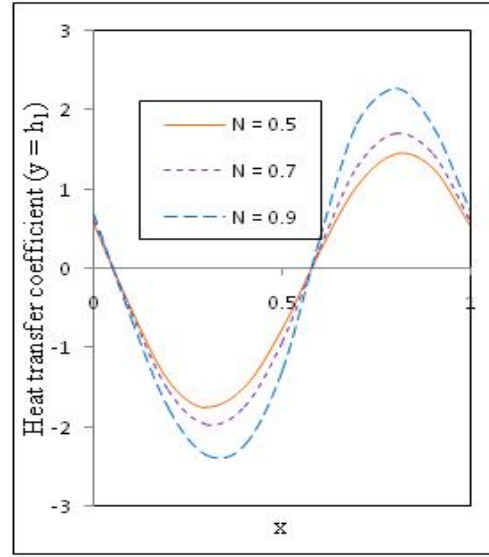


Figure (24): Heat transfer coefficient ( $y = h_1$ ) for different values of  $N$  with fixed  $M = 1$ ,  $Da = 0.3$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

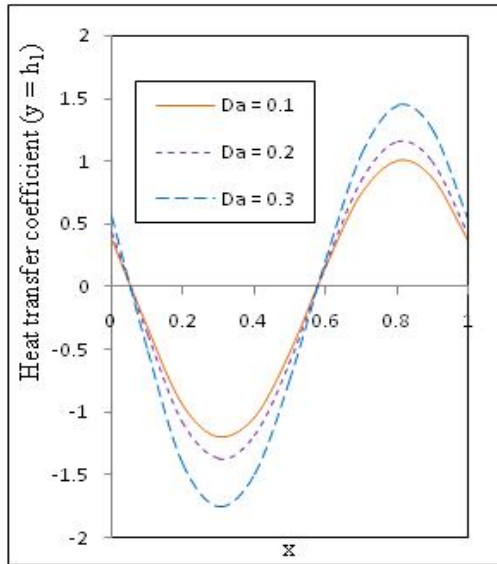


Figure (23): Heat transfer coefficient ( $y = h_1$ ) for different values of  $Da$  with fixed  $M = 1$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

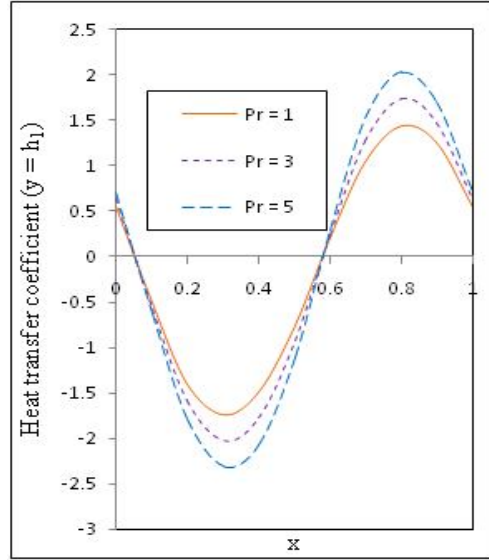


Figure (25): Heat transfer coefficient ( $y = h_1$ ) for different values of  $Pr$  with fixed  $M = 1$ ,  $Da = 0.3$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

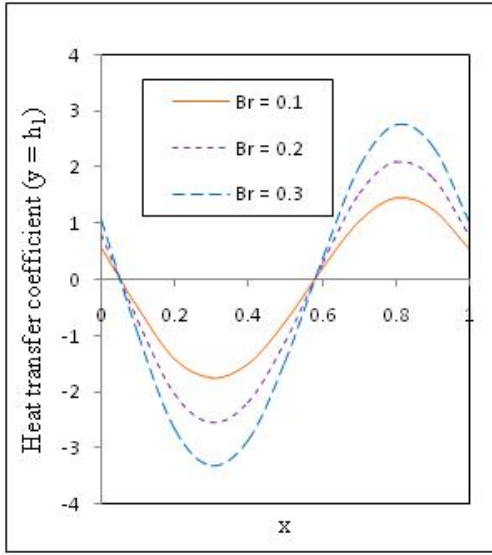


Figure (26): Heat transfer coefficient ( $y = h_1$ ) for different values of  $Br$  with fixed  $M = 1$ ,  $Da = 0.3$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $Pr = 1$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\eta = 0.5$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

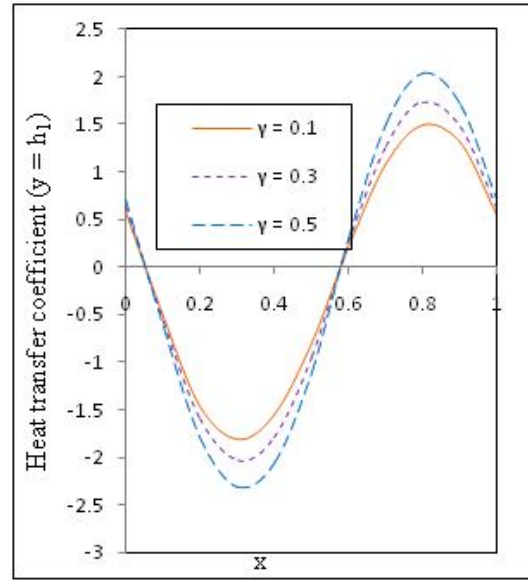


Figure (28): Heat transfer coefficient ( $y = h_1$ ) for different values of  $\gamma$  with fixed  $M = 1$ ,  $Da = 0.3$ ,  $N = 0.5$ ,  $Pr = 1$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\eta = 0.5$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

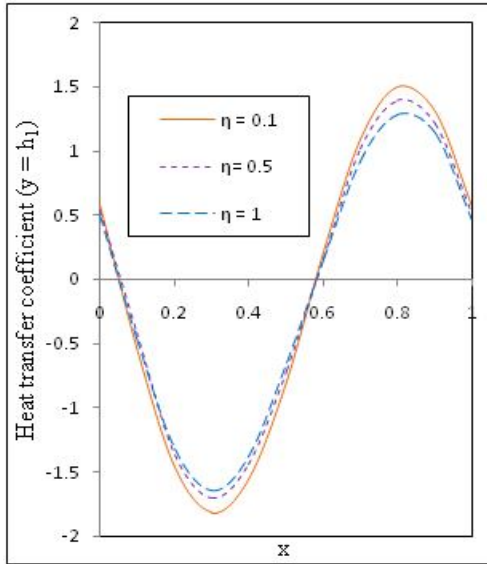


Figure (27): Heat transfer coefficient ( $y = h_1$ ) for different values of  $\eta$  with fixed  $M = 1$ ,  $Da = 0.3$ ,  $N = 0.5$ ,  $\gamma = 0.1$ ,  $Pr = 1$ ,  $Br = 0.1$ ,  $\beta = 0.7$ ,  $\phi = \pi/6$ ,  $\alpha = \pi/6$ ,  $\varepsilon = 0.2$ ,  $k_1 = 0.1$ ,  $t = 0.4$ ,  $p = 0.5$

## Conclusions

An influence of slip and joule heating on MHD peristaltic blood flow with uniform porous medium through an inclined asymmetric vertical tapered channel in the presence of radiation -blood flow model. The important findings of the present study are summarized below.

- (1) Axial velocity increases with increase in  $M$ ,  $\beta$ ,  $\eta$  and  $\alpha$ .
- (2) Axial velocity decreases with increase in  $Da$ .
- (3) Pressure gradient enhances with increase in  $M$ ,  $\beta$ ,  $\eta$  and  $\alpha$ .
- (4) Pressure gradient decreases with increase in porous parameter ( $Da$ ) and Volumetric

flow rate ( $\bar{Q}$ ).

- (5) Temperature distribution increases with increase in  $M$ ,  $Pr$ ,  $Da$ ,  $N$ ,  $\alpha$  and  $Br$ .
- (6) Temperature distribution decreases with increase in  $\beta$  and  $\eta$ .
- (7) Heat transfer coefficient increases in the portion of the inclined tapered channel  $x \in [0, 0.05]$   $U [0.58, 1]$  and it decreases in the other portion of the inclined tapered channel  $x \in [0.05, 0.58]$  with increase in  $M$ ,  $Pr$ ,  $Da$ ,  $N$ ,  $\gamma$  and  $Br$

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